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2 **Biodiesel Production from Tigernut (*Cyperus esculentus*) Oil**
3 **and Characterization of its Blend with Petro-diesel**

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5 **Ofoefule, A.U^{*1}., Ibeto, C.N¹., Okoro, U.C² and Onukwuli, O.D³**

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7 ¹National Centre for Energy Research and Development, University of Nigeria, Nsukka.

8 ² Department of Pure and Industrial Chemistry, University of Nigeria Nsukka, Enugu state.

9 ³Department of Chemical Engineering, Nnamdi Azikiwe University Awka, Anambara state

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14 **ABSTRACT (ARIAL, BOLD, 11 FONT, LEFT ALIGNED, CAPS)**

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This study was carried out to assess the fuel quality of biodiesel produced from tigernut (*Cyperus esculentus*) oil and its blends with petro- diesel. The oil was extracted from the tigernut by solvent extraction method using petroleum ether. The oil was trans-esterified using potassium methoxide at the temperature of 60°C for 60 min at a catalyst concentration of 0.65% and under a constant stirring speed. The crude biodiesel obtained was purified by washing with water and subsequently dried in an oven. The biodiesel was again blended with petro- diesel to obtain various blends of B10, B20, B30 and B40. Oil and biodiesel yields were assessed while physicochemical analysis of the oil, biodiesel and blends were carried out using standard methods for physicochemical parameters including flash point, cloud point and pour point. Results obtained showed that the oil yield from the feedstock was 16%, while the biodiesel yield was 82%. The high and moderate flash points of the biodiesel and blends ranged between 90-178°C, their cloud points ranged between 6.5-13°C while their pour points ranged between -3-(-10)°C. General results of the blends showed that B10 and B20 had performance results closer to petro-diesel and ASTM standards. Therefore, the blends, in addition to being good for biodiesel engines, would also be suited for engines not specifically designed for biodiesel use.

16
17 *Keywords:* Tigernut, transesterification, biodiesel, biodiesel blends, petro-diesel

18
19 **1. INTRODUCTION**

20
21 Currently there is a strong interest in biodiesel, mainly driven by growing volatility in global
22 crude oil markets and concerns over climate change and the desire to address the global

*Corresponding Author

E-mail: akuzuoo@yahoo.com

Tel: +234-8036798570

23 risk. Biodiesel has proven to be a good substitute for petroleum diesel in motor vehicles and
 24 generators, when it meets the international standards such as ASTM for automotive use.
 25 Biodiesel is biodegradable, non-toxic and has low emission profiles when compared to fossil
 26 fuel and its usage will allow balance between agriculture, economic development and the
 27 environment [1]. Biodiesel is produced through a chemical process known as trans-
 28 esterification. Transesterification of vegetable oils with low molecular weight simple alcohols
 29 (methanol, ethanol, propanol, butanol and amyl alcohol) has been established as the best
 30 option to reduce the high viscosity, low volatility, heavy engine deposits and toxic substance
 31 formation associated with the direct use of vegetable oils [2, 3]. Tigernut is not really a nut
 32 but a small tuber that was discovered some 4000 years ago. It has been cultivated both as
 33 livestock feed and for human consumption. It is widely grown in Florida US, Spain, Britain,
 34 China, Mali and Ivory Coast. The plant is widely distributed in West Africa where it is
 35 cultivated mainly for the edible tubers which it bears underground [4]. In northern Nigeria, the
 36 tubers of tigernut can be bought in the market all year round. Table 1 shows the fatty acid
 37 composition of tigernut.

38
 39 **Table 1: Fatty acid composition of Tigernut oil**

Tigernut oil	Fatty acid composition (%)
Oleic	75.72
Linoleic	11.64
Palmitic	10.21
Stearic	1.47
Linolenic	0.64
Arachidic	0.32

41 **Source: Temple [4]**

42
 43 Many research works have explored commercially edible oils like cotton seed oil, sun flower
 44 seed oil, soybean oil, peanut oil, coconut oil and palm oil as the feedstock for biodiesel [5, 6],
 45 however, availability of these raw materials varies. Although tigernut oil is from an edible
 46 feedstock, its use as a potential feedstock for biodiesel production may not likely compete
 47 with its use as food since it is not a staple food or widely consumed [7]. Most parts of the
 48 tropics are suitable for biofuel crops cultivation including tigernut. This strategy to use crops
 49 of relative abundance in a particular region for biofuel production is effectively being
 50 employed in USA and Brazil as they are the world largest producers of bioethanol from
 51 Sugarcane and other raw materials [8]. Currently, tigernut use in Nigeria is mainly for

52 production of milk juice and as snacks etc. However, the tuber can be used for other
53 numerous purposes aside consumption as food. It has been reported to serve effectively as
54 a supplementary feedstock for biodiesel production [9]. The high fibre content makes it
55 useful for pyrolysis / gasification to biofuels, the moderate starch content also makes it a
56 potential supplementary feedstock for bioethanol production [10]. The wastes emanating
57 from its processing also makes it a veritable feedstock for biogas production under
58 anaerobic digestion [10].

59 Some studies have been carried out on biodiesel production from tigernut. Barminas *et al.*
60 [11], carried out preliminary studies of transesterification of tigernut (*Cyperus esculentus*) as
61 a source of biofuel. Also, Ugheoke *et al.* [9] studied the optimization of the transesterification
62 process of tigernut oil for biodiesel production, specifically to determine the optimal catalyst
63 concentration level that gives maximum yield of methyl ester (biodiesel) from the oil. Again,
64 Salau *et al.* [12] examined the proximate composition, food functionality and oil
65 characterization of mixed varieties of tigernut rhizome flour and reported oil yields ranging
66 between 25 and 34%.

67 Most parts of the world use a system known as the 'B' factor to state the amount of biodiesel
68 in any mix [13]. For instance, pure biodiesel is referred to as B100 while B20 is 20%
69 biodiesel and 80% petro-diesel. However, taking U.S as a case study, biodiesel is mostly
70 blended with diesel fuel. Such a blend would have better cold flow properties when
71 compared with neat biodiesel. Consequently, blending biodiesel with petro-diesel may be
72 advantageous for mitigating the poor cold flow properties of biodiesel from many lipid
73 feedstocks. On the other hand, blending at higher ratios may compromise cold flow
74 properties [14]. Again, biodiesel contains no petroleum, but it can be blended with petroleum
75 diesel in any percentage. Biodiesel blends from 2 percent to 20 percent (representing B2
76 and B20 respectively) can be used in most diesel engines with minor or no modifications.
77 This study therefore aimed to determine the fuel quality of biodiesel produced from methyl
78 esters of tigernut (*Cyperus esculentus*) and its blends with petro-diesel. This was also done
79 in order to determine the most suitable blending ratio for biodiesel produced from tigernut
80 seed oil with petro-diesel and also determine if higher blending ratios differ considerably in
81 quality from lower blending ratios.

82

83 2. MATERIALS AND METHODS

84

85 2.1. Materials

86 Fresh tigernut was purchased from a local market in Enugu town of Enugu State, Nigeria.
87 Analytical grade reagents were used for all the analyses carried out without further
88 purification. The petroleum ether was used as procured without further purification. The

89 Methanol used was a product of Merck, Darmstadt, Germany (99.7% purity), while the
90 potassium hydroxide was a product of Loba Chemie GmbH Switzerland (85% purity). Other
91 materials also used were fractionating column, aluminium foil, 1L beakers, 1.5L biodiesel
92 reactor (fabricated locally), thermo- regulator heater equipped with stirrer (Heizung
93 Chauffage, MGW- LAUDA, D6970, Lauda- Königshofen, Germany), electronic digital
94 weighing balance (Ohaus, Adventurer, model- AR 3130), specific gravity bottle, pH meter
95 (Hanna pH meter model No. 02895), Rotary evaporator, oven (BTOV 1423), Vecstar furnace
96 LF3, Ferranti portable viscometer model VL, Abbe refractometer, semi automatic Cleveland
97 flash point tester and Hewlett Adiabatic Bomb Calorimeter model 1242. The study was
98 carried out in the National Centre for Energy Research and Development, University of
99 Nigeria Nsukka in August, 2010.

100

101 **2.2. Oil extraction**

102 The tigernut was washed with water to remove sand particles adherent in the tuber and then
103 allowed to dry. The seeds were ground into coarse particle sizes with a mechanical grinder
104 (local mill) and placed in a solar dryer for four days to remove residual moisture. The dried
105 meal was packed in a big fractionating column up to three quarter level and petroleum ether
106 was poured well above the level of the meal in the column. It was closed with aluminium foil
107 and masking tape and then left for a period of 8 h. The mixture of oil and solvent was
108 collected from the bottom of the column with a beaker. This was repeated to extract more
109 the oil from the meal. The oil was recovered using rotary evaporator to distil off the solvent.
110 After the distillation, the oil was left in the open to totally dry up completely.

111

112 **2.3. Characterization of oil**

113 The oil was characterized for pH using a pH meter, specific gravity using a specific gravity
114 bottle, moisture content by the oven dry method, ash content by heating to dryness in
115 furnace, kinematic viscosity using a viscometer, the acid value, saponification value, Iodine
116 value and Peroxide value by titrimetry, refractive index using Abbe refractometer [15] and
117 percentage free fatty acid (% FFA, as oleic) was determined by multiplying the acid value
118 with the factor 0.503. Thus % FFA = 0.503 x acid value [16].

119

120 **2.4. Physicochemical analyses**

121 Ash, moisture, fibre and calorific values were determined using AOAC method [17]. Fat,
122 crude nitrogen and protein contents were determined using Soxhlet extraction and micro-
123 Kjeldhal methods described in Pearson [18]. Carbohydrate content was determined by
124 difference [19].

125 **2.5. Preparation of Potassium Methoxide**

126 250 ml of methanol was measured into a 500 ml flat bottom flask and covered immediately.
127 5.8 g of potassium hydroxide was carefully added into the methanol to make a solution
128 which was made airtight. It was shaken and swirled for a few times until the potassium
129 hydroxide was completely dissolved. This gave a catalyst concentration of 0.65%.

130

131 **2.6. Biodiesel production and purification**

132 The transesterification reaction was carried out in a 1.5L airtight biodiesel reactor vessel
133 fitted with thermo-regulator heater/ stirrer. One litre of tigernut oil was measured into the
134 flask and was heated to a temperature of 60°C. The potassium methoxide was then poured
135 into the flask containing the oil and was immediately covered. The temperature of the system
136 was maintained at 55-60°C for the one hour duration of the reaction. At the end of the
137 reaction, the mixture was transferred into a separatory flask, left for 24 h and then the
138 biodiesel separated from the glycerol by gravity. The biodiesel was purified by washing with
139 water five times to obtain a clear water and neutral pH [20, 21]. The glycerol was not refined
140 further but was kept for other uses.

141

142 **2.7. Characterization of biodiesel and its blend**

143 The different blends; B10, B20, B30 and B40 were prepared by mixing 10, 20, 30 and 40 ml
144 biodiesel and 90, 80,70,60 ml petro-diesel respectively. They were analyzed in the same
145 way as the tigernut oil for the same parameters and also calorific value using a Bomb
146 calorimeter, flash point using a semi automatic Cleveland flash point tester via the American
147 system of testing materials (ASTM D93), cloud point (ASTM D2500) and pour point (ASTM
148 D97) methods.

149

150 **3. RESULTS AND DISCUSSION**

151

152 Table 2 shows the proximate composition of the tigernut tuber and starch after de-oiling of
153 the feedstock, while Table 3 shows the physic-chemical properties of the tigernut oil. The
154 calorific value, carbohydrate content and fat content of the tuber indicate that the feedstock
155 would serve as a good source for biofuels production since the inherent energy content
156 would increase the burning power.

157

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160

161 **Table 2: Proximate composition of tigernut tuber and starch**

Parameters	Tigernut tuber	Tigernut starch
Oil yield (%)	15.91	n/a
Moisture (%)	5.77	8.13
Ash (%)	1.86	6.14
Crude fibre (%)	9.50	7.98
Crude fat (%)	25.70	2.33
Crude nitrogen	1.12	0.52
Crude protein (%)	7.00	3.24
Carbohydrate (%)	65.50	65.18
Calorific value(kcal/g)	524.60	345.88

162

163 As shown in Table 2, the oil yield from the tigernut was approximately 16% which is quite low
 164 when compared with most oil seed feedstock (Peanut- 50%, Sesame seed- 50%, olive seed-
 165 40% Almond- 50%, castor seed- 50% sunflower seed- 35% etc.) [22]. However, by- product
 166 of the tuber after extraction can be put to good use as feedstock for other biofuels
 167 production/application. The odour and clear golden yellow colour of the oil are favourable for
 168 aesthetic qualities.

169

170 **Table 3: Physico-chemical properties of tigernut oil**

Parameters	Results
Odour	Odourless
Colour	Yellow
Specific gravity	0.91
pH	5.30
Moisture (%)	5.32
Ash content (%)	2.60
Iodine value (g/100g)	143.37
Acid value (mg/KOHg ⁻¹)	8.97
Saponification value (mg/KOHg ⁻¹)	161.54
Peroxide value (mEq/Kg)	8.33
Free fatty acid (%)	4.49
Viscosity (mm ² /s)	0.98
Refractive index	0.77

171

172 Acid values of the oil and biodiesel were very high and exceeded the ASTM standard of 0.8
 173 mg/KOHg⁻¹ (Tables 3 and 4). Vegetable oils containing high free fatty acids have significant
 174 effects on the transesterification with methanol using alkaline catalyst. It also interferes with
 175 the separation of fatty acid ester and glycerols [23]. This also may have affected the yield of
 176 biodiesel which was lower than most high yielding ones (95% and above). For instance,
 177 Highina *et al.*, [24] reported 97% biodiesel yield from *Jatropha curcas* while Meka *et al.* [25]
 178 reported 96.85 biodiesel yield from Safflower. Even though the biodiesel yield was lower

179 than more favourable yield of 95% and above, it was however higher than that obtained for
 180 peanut oil reported by Itodo *et al.* [26] (50%) and Ibeto *et al.* [8] (79%). The low pH level
 181 observed in the oil and the high free fatty acid content (Table 3) shows that it is acidic. This
 182 may be responsible for the poor conversion efficiency of the oil to biodiesel. This also
 183 suggests that the oil may require the two stage method of either esterification followed by
 184 transesterification or saponification followed by transesterification. This will ensure proper
 185 pre-treatment of the oil and increase biodiesel yields [27].

186 The specific gravities of the B100 and the blends were within the range and compared with
 187 that of biodiesel from other oil sources. Densities and other gravities are important
 188 parameters for diesel fuel injection systems. The values must be maintained within tolerable
 189 limits to allow optimal air to fuel injection systems.

190

191 **Table 4: Physicochemical properties of petro-diesel, biodiesel and biodiesel blends**

Parameters	Petro diesel	B100	B10	B20	B30	B40	ASTM Std
Biodiesel yield (%)	-	82					≥ 95
Specific gravity	0.85	0.87	0.86	0.86	0.85	0.85	0.875-0.90
Ash content (%)	-	1.13	1.53	1.53	1.20	2.0	0.01 max
Iodine value (g/100g)	-	98.38	90.35	90.35	90.46	90.46	120 max
Acid value (mg/KOHg ⁻¹)	-	1.122	1.683	1.724	2.805	2.68	0.05 max
Saponification value(mg/KOHg ⁻¹)	-	108.46	106.74	106.73	104.49	103.37	
Free fatty acid (%)	-	0.56	0.84	0.86	1.40	1.34	
Viscosity (mm ² /s)	5.51	8.08	5.54	5.61	5.84	5.68	1.9-6.0
Refractive index	-	0.77	0.86	0.75	0.77	0.86	
Calorific value (J/g)	22,905	-	15,140	26,851.	32,545	19,736	
Flash point (°C)	-	178	120	110	92	90	93 min.(US)
Cloud point (°C)	-	13	11	9	6.5	8.0	
Pour point (°C)	-	-3	-7	-9	-10	-9	-10

192

193 The ash content of both the B100 and the blends were well above the ASTM standard. This
 194 indicates that it may likely have higher mineral contents leading to some level of air
 195 pollutants like SO_x and NO_x.

196 The viscosity of the B100 was slightly higher than the ASTM standard. However, the blends
 197 fell within the range required for use in the engines. They also compared well with the petro-
 198 diesel whose viscosity was 5.51mm²/s. However, B10 and B20 had lower values than the
 199 other blends. The iodine values were within standard. Higher iodine values indicate high

200 unsaturation in oils and fats. The values obtained in the B100 and blends showed that the
201 unsaturation was taken care of by transesterification. There was no reasonable difference
202 between the values obtained for the different blends. Saponification value is used for
203 checking **impurities**. The saponification value for the B100 and the blends were lower when
204 compared with that obtained for peanut oil (244.74 and 218.09 mg/KOHg⁻¹) and the Jatropha
205 oil seed which was 193.55mgKOHg⁻¹ as reported by Akbar *et al.*, [28]. This indicates that the
206 level of **impurities** in the tigernut oil biodiesel was very low.

207 The flash point of the B100 and blends except **B30 and B40** were actually within the ASTM
208 6751 standard specification of 93°C set in order for the biodiesel to be classified as a non-
209 hazardous material for shipping in the United States. This indicates that with their use, the
210 fear of fire outbreaks would be eliminated. The value of the flash point for B30 and B40
211 indicate that they may not be very good blends for use **since they did not fall within the**
212 **ASTM standard range**. The cloud point and the pour point of both the B100 and the blends
213 were well within the standard. One of the problems associated with biodiesel is its cold flow
214 properties represented by the pour point. The pour point is the lowest temperature at which
215 frozen oil can flow and is used to specify the cold temperature instability of fuel oil. This
216 shows that biodiesel from tigernut oil would perform very well in very cold and temperate
217 regions. This also indicates that countries in the tropics where cultivation of tigernut thrives,
218 can exploit this outlet into biofuels crop cultivation in order to export the oil to western
219 countries for the purposes of biofuels production. They all also showed **good** calorific values.
220 This indicates that they would burn with high release of energy.

221
222

223 **4. CONCLUSION**

224

225 The study has shown that tigernut is a good supplementary feedstock for biodiesel
226 production. The results of the blends of the petro-diesel with tigernut biodiesel showed that
227 that B10 and B20 had results closer to B100 and to the ASTM standards and would give
228 better performance than B30 and B40. **Therefore, the blends, in addition to being good for**
229 **biodiesel engines, would also** be suited to engines not specifically designed for biodiesel
230 use. This compares very well with biodiesel from other oil sources. Even though tigernut oil
231 is edible oil, the crop is not consumed on a large scale as a staple food and it is not also a
232 major source of edible oil, so it would be advisable if countries in the tropics **including Nigeria**
233 consider the cultivation of this crop on a large scale. If this is achieved, it would facilitate the
234 use of tigernut for biodiesel production on a large scale and hence alleviate the global
235 concern for food security.

236

237 **AUTHORS' CONTRIBUTIONS**

238

239 The first and corresponding author designed the study and wrote the protocol. Author 1
240 carried out the experimental studies. Author 2' wrote the first draft of the manuscript. 'Author
241 1' and 2' managed the analyses of the study while Authors 3' and 4' supervised the overall
242 work. All authors approved the final manuscript."
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245 **REFERENCES**

246

247 [1] Meher LC, Sagar DV, Naik SN. Technical Aspect of Biodiesel Production by
248 Transesterification- A Review. Renewable Sustainable Energy Rev. 3; 2004.

249

250 [2] Schwab AW, Baghy MO, Freedman B. Preparation and properties of Diesel fuel from
251 vegetable oils. Fuel, 1987; 66: 1372 – 1378.

252

253 [3] Tesser R, Di Serio M, Guida M, Nastasi M, Santacesaria E. Kinetics of Oleic acid
254 etherification with methanol in the presence of Triglycerides. Ind. Eng. Chem. Res., 2005;
255 44: 7978- 7982.

256

257 [4] Temple VJ. Lesser Known Plant Foods. In: Nutritional quality of plant foods A. U. Osagie
258 and O. U. Eka (Eds.) Post harvest Research Unit, Department of Biochemistry, University of
259 Benin. Benin City. Nigeria, 1998.

260

261 [5] Syam AM, Yunus R, Ghazi TIM. Yaw TCS. Methanolysis of jatropha oil in the presence
262 of potassium hydroxide catalyst. J. Applied Sci., 2009; 9: 3161-3165.

263

264 [6] Ofoefule AU, Ibeto CN, Ugwu LC, Eze DC. Determination of Optimum Reaction
265 Temperature and Reaction Time for Biodiesel yield from Coconut (*Cocos nucifera*) oil. In
266 proc. International workshop on Renewable Energy for sustainable Development in Africa
267 (IWRESDA). Nondon Hotel, Enugu. 5th – 7th November, 2012.

268

269 [7] Bamishaiye EI, Bamishaiye OM. Tigernut as a plant, its derivative and benefits. Afr. J.
270 Food, Agric, Nutr. & Dev., 2011; 11(5): 5157-5170.

271

272 [8] Ibeto CN, Ofoefule AU, Ezeugwu HC. Fuel Quality Assessment of Biodiesel Produced
273 from Groundnut Oil (*Arachis hypogea*) and its blend with petroleum diesel. Amer. J. Food
274 Tech. 2011 6(9): 798-803.

275

276 [9] Ugheoke BI, Patrick DO, Kefas, HM, Onche EO. Determination of Optimal Catalyst
277 Concentration for Maximum Biodiesel Yield from Tigernut (*Cyperus esculentus*) Oil.

278 [Leonardo Journal of Sciences](#), 2007; 6(10): 131 - 136.

279

280 [10] Ofoefule AU. Biofuels potentials of some biomass feedstock for bioethanol and biogas.
281 PhD Thesis. University of Nigeria, Nsukka. 2012.

282

283 [11] Barminas JT, Maina HM, Tahir S, Kubmarawa D, Tsware K. A preliminary investigation
284 into the biofuel characteristics of tigernut (*Cyperus esculentus*). Bioresour. Technol., 2001;
285 79: 87-89.

286

287 [12] Salau RB, Ndamitso MM, Paiko YB, Jacob JO, Jolayemi, OO, Mustapha S. Assessment
288 of the proximate composition, food functionality and oil characterization of mixed varieties of
289 *Cyperus esculentus* (Tigernut) rhizome flour. Cont. J. Food Sci & Tech.(2012); 6(2): 13-19.

- 290 [13] Knothe G. Analytical methods used in the production and fuel quality assessment of
291 biodiesel. *Trans. ASAE*, 2001;44: 193-200.
292
- 293 [14] Dunn RO. Improving the Cold Flow Properties of Biodiesel by Fractionation,
294 Soybean - Applications and Technology, Tzi-Bun Ng (Ed.), ISBN: 978-953-307-207-4,
295 InTech, Available from: [http://www.intechopen.com/books/soybean-applications-and](http://www.intechopen.com/books/soybean-applications-and-technology/improving-the-cold-flow-properties-of-biodiesel-by-fractionation)
296 [technology/improving-the-cold-flow-properties-of-biodiesel-by-fractionation](http://www.intechopen.com/books/soybean-applications-and-technology/improving-the-cold-flow-properties-of-biodiesel-by-fractionation). Accessed
297 13/11/2012
298
- 299 [15] Van Gerpen JH. Biodiesel processing and production. *Fuel Processing Technology*,
300 2005; 86 (10): 1097–1107.
301
- 302 [16] Ejiloh IR, Asere AA. Tested performance parameters of Transesterified sheanut oil and
303 diesel fuel blends in compression ignition engines. In proc. National Solar Energy Forum
304 (NASEF). University of Agriculture, Makurdi. Benue state. 2010: 1-14.
305
- 306 [17] AOAC. Official methods of Analysis. Association of Analytical Chemists. 14th ed.
307 Washington, USA. 22209. 2010.
308
- 309 [18] Pearson D. The Chemical Analysis of Foods (7th Ed.), Churchill Livingstone. New York,
310 1976.
311
- 312 [19] Onwuka GI. Food Analysis and Instrumentation (theory and practice). Naphtali prints,
313 Nigeria. 2005
- 314
- 315 [20] Alamu OJ, Waheed MA, Jekayinfa SO. Biodiesel Production from Nigerian Palm
316 Kernel Oil: Effect of KOH Concentration on Yield”, *Energy for Sustainable Development*,
317 XI, 2007; 3:77-82.
318
- 319 [21] Chitra P, Venkatachalam P, Sampathrajan A. Optimization of experimental
320 conditions for biodiesel production from alkali catalysed transesterification of *Jatropha*
321 *curcas* oil. *Energy for Sustainable Development*. 2005; 9 (3): 13-18.
322
- 323 [22] Casten J, Snyder HE. Understanding pressure extraction of vegetable oils. Volunteers in
324 Technical Assistance (VITA). Technical paper No. 40. Sourced at
325 <http://www.enterpriseworkers.org/pdfs/VITA%20publication%20catalogues.pdf>. Accessed
326 02/07/2010.
327
- 328 [23] Ma F, Hanna MA. Biodiesel production: a review. *Bioresource Technol*, 1999; 70 (1): 1–
329 15.
330
- 331 [24] Highina BK, Bugaje IM, Umar B. Biodiesel production from *Jatropha curcas* oil in a
332 batch reactor using zinc oxide as catalyst. *J. Appl. Phytotech. Environ. Sanit.*, 2012; 1(6): 61-
333 66.
334
- 335 [25] Meka PK, Tripathi V, Singh RP. Synthesis of biodiesel fuel from safflower oil using
336 various reaction parameters. *J. Oleo Sci.*, 2007; 56 (1): 9-12.
337
- 338 [26] Itodo IN, Oseni MI, Wergba C. A comparative study of the properties and yield of
339 biodiesel from soy and groundnut oils. *Nig. J. Solar Ener.* 2009; 21:124-128.
340

- 341 [27] Jansri S, Prateepchaikul G. Comparison of biodiesel production from high free fatty acid,
342 crude coconut oil via saponification followed by transesterification or a two-stage process.
343 Kasetsart J. Nat. Sci., 2011; 45: 110 – 119.
344
- 345 [28] Akbar E, Yaakob Z, Kamarudin SK, Ismail M, Salimon J. Characteristics and
346 composition of (*Jatropha curcas*) oil seed from Malaysia and its potential as biodiesel
347 feedstock. Eur. J. Sci. Res., 2009; 29(3):396-403.